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## SOLITONS IN A DOWN-FLOWING FILM WITH MODERATE MASS FLOW RATES OF THE LIQUID

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Using the hypothesis of self-similarity, in [1] an equation was obtained describing long-wave perturbations in a vertical film of liquid with moderate mass flow rates:

$$\left(\frac{\partial}{\partial t} + 3\frac{\partial}{\partial x}\right)h + 6h\frac{\partial h}{\partial x} - \frac{2}{15}\text{Re}\frac{\partial}{\partial t}\left(h\frac{\partial h}{\partial t}\right) + \frac{\text{Re}}{3}\left(\frac{\partial}{\partial t} + 1.69\frac{\partial}{\partial x}\right)\left(\frac{\partial}{\partial t} + 0.71\frac{\partial}{\partial x}\right)h + W\frac{\partial^4 h}{\partial x^4} = 0, \quad (1)$$

where  $\text{Re} = gh_0^3/3\nu^2$ ;  $W = \sigma/\rho h_0^2$ ;  $h$  is the shift of the surface of the film from the unperturbed level, measured in units of  $h_0$ ; and  $h_0$  is the thickness of the unperturbed film.

For a steady-state running wave  $h = h(x - ct)$ , from (1) we obtain

$$(3 - c)h' + 6hh' - 2\text{Re}c^2(hh')'/15 + \text{Re}(1.69 - c)(0.71 - c)h''/3 + Wh^{IV} = 0 \quad (2)$$

(a prime means differentiation with respect to  $x$ ).

In finding soliton solutions of Eq. (2), it can be integrated once:

$$(3 - c)h + 3h^2 - 2\text{Re}c^2hh'/15 + \text{Re}(1.69 - c)(0.71 - c)h'/3 + Wh^{IV} = 0. \quad (3)$$

Using the replacement

$$h = aH, \quad x_1 = bx, \quad (4)$$

$$a = Wb^3, \quad b = (\text{Re}(1.69 - c)(0.71 - c)/3W)^{1/2}$$

Eq. (3) is brought to the form

$$-c_1H + 3H^2 - 2mHH' - H' + H''' = 0, \quad (5)$$

where

$$c_1 = (c - 3)(3(z(1.69 - c)(0.71 - c)))^{3/2}, \quad (6)$$

$$m = c^2z((1.69 - c)(0.71 - c)/3)^{1/2}/15, \quad z = (\text{Re}^3/W)^{1/2}.$$

Relationships (4)-(6) are valid if

$$c > 1.69 \quad \text{or} \quad c < 0.71.$$

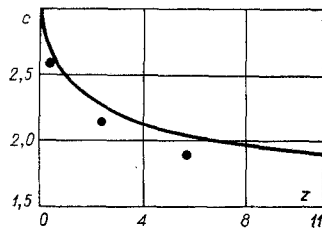


Fig. 1

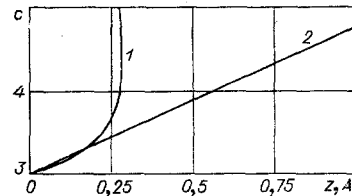


Fig. 2

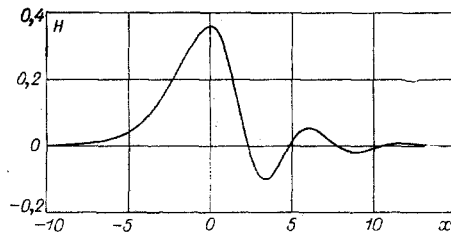


Fig. 3

Thus, the problem is brought down to the solution of Eq. (5); for a given value of  $m$ , the eigenvalue  $c_1$  and the soliton function  $H$  are found. The values of the velocities of the solitons  $c$  and the corresponding values of  $z(c)$  are found from (6), and of the function of  $h$ , from (4).

Representing the soliton solution of Eq. (5) in the form of a Fourier integral

$$H = \int H_k \exp(ikx_1) dk,$$

for determination of  $H_k$  we obtain the integral equation

$$H_k = (3 - ikm) \int H_k H_{k-k'} dk' / (c - i(k - k'^3)). \quad (7)$$

By virtue of the invariance of Eq. (5) with respect to the replacement

$$c_1 \rightarrow -c_1, H \rightarrow -H, x_1 \rightarrow -x_1, m \rightarrow -m$$

it is sufficient to consider only the region of values of the parameter  $m \geq 0$ . Equation (7) was solved by a method described in [2].

Depending on whether the value of  $\int_{-\infty}^{\infty} h dx$  is greater or less than zero, the value of a soliton is relatively positive or negative.

Figure 1 gives the dependence of the velocity of negative solitons on the parameter  $z$ . For purposes of comparison, the points plot the data of [3], in which soliton solutions close to Eq. (2) are sought.

Figure 2 gives values of the velocities of the positive solitons found, as a function of  $z$  (curve 1). Such solitons can exist only with values of  $z \leq z_* = 0.2810$ . Curve 2 gives the dependence of the amplitudes of these solitons on their velocity. Here  $A \equiv (H_{\max} - H_{\min})a$ . For  $z = z_*$  the form of a soliton is shown in Fig. 3. Its velocity  $c = 4.405$ , and its amplitude  $A = 0.784$ .

For the case  $z \ll 1$ , soliton solutions were found in [2]. With finite values of the parameter  $z$ , positive solitons have not been observed earlier, although they are of great interest, since, in an experiment, wavy conditions are attained in the form of a sequence of positive solitons [4]. The presence of  $z_*$  makes it easier to understand why the thickness of the residual layer, over which these solitons are propagated, depends only slightly on the mass flow rate of the liquid  $Q$ . If the value of  $Q$  is such that  $z > z_*$ , the flow is restructured in such a way that the value of the parameter  $z$ , calculated from the thickness of the residual layer, is of the order of  $z_*$ , and the residual mass flow rate goes over into solitons. Thus, knowing  $z_*$  and  $Q$ , the number of solitons arising and the fraction of sections of the film with a flat boundary can be evaluated.

Such an evaluation can be useful for a number of problems of heat and mass transfer through the surface of a film.

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## UNSTEADY ROTATION OF A CYLINDER IN A VISCOUS FLUID

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The flow of a viscous fluid around a cylinder set in rotational motion at constant angular velocity was investigated in [1, 2]. The present paper deals with the problem of rotation, in a viscous incompressible fluid, of a round cylinder, on unit length of which, beginning at time  $t = 0$ , there acts a constant moment of external forces  $M$ . The fluid flow is assumed to be plane. At  $t \leq 0$  the cylinder and fluid are at rest.

We select cylindrical coordinates  $r, \theta$ , and  $z$  in such a way that the  $z$  axis is directed along the cylinder axis. We assume that the flow velocity  $V$  is independent of  $\theta$ . Then, as is easily verified, the  $r$  component of the vector  $V$  is zero, and the considered problem reduces to solution of the equations

$$\frac{\partial V_\theta}{\partial t} = \nu \left( \frac{\partial^2 V_\theta}{\partial r^2} + \frac{1}{r} \frac{\partial V_\theta}{\partial r} - \frac{V_\theta}{r^2} \right); \quad (1)$$

$$I \frac{d\Omega}{dt} = M + L \quad (2)$$

with the following initial and boundary conditions:

$$V_\theta = 0 \text{ when } t = 0, r \geq a; \quad (3)$$

$$V_\theta = a\Omega \text{ when } r = a; \quad (4)$$

$$V_\theta \rightarrow 0 \text{ when } r \rightarrow \infty, \quad (5)$$

where  $V_\theta$  is the  $\theta$  component of vector  $V$ ;  $I$  is the moment of inertia of unit length of the cylinder;  $\Omega$  is the angular velocity of the cylinder;  $a$  is the radius of the cylinder;  $\nu$  is the kinematic viscosity;  $L = 2\pi\mu a^2(\partial V_\theta/\partial r|_{r=a} - \Omega)$  is the moment of viscous forces acting on unit length of the cylinder due to the fluid;  $\mu = \rho\nu$ ;  $\rho$  is the density of the fluid.

To solve the posed problem we use an operational method. Converting to images in (1), (2), (4), and (5), we obtain

$$\frac{\partial^2 V_\theta^*}{\partial r^2} + \frac{1}{r} \frac{\partial V_\theta^*}{\partial r} - \left( \frac{1}{r^2} + \frac{p}{\nu} \right) V_\theta^* = 0; \quad (6)$$

$$Ip\Omega^* = M^* + L^*; \quad (7)$$

$$V_\theta^* = a\Omega^* \text{ when } r = a; \quad (8)$$

$$V_\theta^* \rightarrow 0 \text{ when } r \rightarrow \infty, \quad (9)$$

where

$$V_\theta^* = \int_0^\infty e^{-pt} V_\theta dt; \quad \Omega^* = \int_0^\infty e^{-pt} \Omega dt;$$

$$M^* = \frac{M}{p}, \quad L^* = 2\pi\mu a^2 \left( \frac{\partial V_\theta^*}{\partial r} \Big|_{r=a} - \Omega^* \right); \quad (10)$$

$p$  is a complex variable.

The solution of Eq. (6) satisfying conditions (8), (9) has the form

$$V_\theta^* = a\Omega^* \frac{K_1 \left( r \frac{p^{1/2}}{\nu^{1/2}} \right)}{K_1 \left( a \frac{p^{1/2}}{\nu^{1/2}} \right)}, \quad (11)$$

where  $K_1$  is a MacDonal function. Using (7), (10), (11), we obtain